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Finite Element Solution of Thermal Radiation and Mass Transfer Flow past Semi- infinite Moving Vertical Plate with Viscous Dissipation in Presence of heat Source / Sink.

Y. Dharmendar Reddy and V. Srinivasa Rao
Department of Mathematics, Anurag Group of Institutions,
Ghatkesar, R.R.Dist.,Telangana State, India.

Abstract

An analysis is carried out to investigate the radiation effects on unsteady heat and mass transfer flow of a chemically reacting fluid past a semi-infinite vertical plate with viscous dissipation in presence of heat source / sink. The method of solution can be applied for Finite element technique. Numerical results for the velocity, the temperature and the concentration are shown graphically. The expressions for the skin-frication, Nusselt number and Sherwood number are obtained. The results show that increased cooling (Gr>0) of the plate and the Eckert number leads to a rise in the velocity. Also, an increase in the Eckert number leads to an increase in the temperature, Whereas increase in source/sink parameter lead to increase in the velocity and temperature distribution when the plate is being cooled.

Keywords: Heat transfer, Viscous dissipation, Radiation, Chemical reaction, heat source/sink, Finite element technique.

INTRODUCTION

For some industrial applications such as glass production and furnace design in space technology applications, cosmial flight aerodynamics, rocket propulsion systems, plasma physics which operate at higher temperatures, radiation effects can be significant. Soundalgekar and Takhar [1] considered the radiative free convection flow of an optically thin grey-gas past a semi-infinite vertical plate. Radiation effects on mixed convection along an isothermal vertical plate were studied by Hussian and Takhar[2]. Raptis and Perdikis[3] have studied the effects of thermal radiation and free convection flow past a moving vertical plate.

Chamkha et al. [4] analyzed the effects of radiation on free convection flow past a semi-infinite vertical plate with mass transfer. Kim and Fedorov [5] studied transient mixed radiative convection flow of a micro polar fluid past a moving, semi-infinite vertical porous plate. Prakash and Ogulu [6] have investigated an unsteady two-dimensional flow of a radiating and chemically reacting fluid with time dependent suction.

In many chemical engineering processes, There does occur the chemical reaction between a foreign mass and the fluid in which the plate is moving. These processes take place in numerous industrial applications viz., Polymer production, manufacturing of ceramics or glassware and food procession. Das et al. [7] have studied the effects of mass transfer on flow past an impulsively started infinite vertical plate with constant heat flux and chemical reaction.

In all these investigations, the viscous dissipation is neglected. The viscous dissipation heat in the natural convective flow is important, when the flow field is of extreme size or at low temperature or in high gravitational field. Gebhar [8] shown the importance of viscous dissipative heat in free convection flow in the case of isothermal and constant heat flux in the plate. Soundalgekar [9] analyzed the effect of viscous dissipative heat on the two dimensional unsteady, free convective flow past an vertical porous plate when the temperature oscillates in time and there is constant suction at the plate. Israel Cookey et al [10] investigated the influence of viscous dissipation and radiation on unsteady MHD free convection flow past an infinite heated vertical plate in porous medium with time dependent suction.

The heat source/sink effects in thermal convection, are significant where there may exist a high temperature differences between the surface (e.g. space craft body) and the ambient fluid. Heat generation is also important in the context of exothermic or endothermic chemical reaction. In recent years MHD flow problems have become in view of its significant applications in industrial manufacturing processes such as plasma studies, petroleum industries Magneto hydrodynamics power generator cooling of clear reactors, boundary layer control in aerodynamics. Many authors have studied the effects of magnetic field on mixed, natural and force convection heat and mass transfer problems. The effect of free convection on the accelerated flow of a viscous incompressible fluid past an infinite vertical plate with suction has many important technological applications in the astrophysical, geophysical and engineering problems. The heating of rooms and buildings by the use of radiators is a familiar example of heat transfer by free convection. Radiation effects on unsteady MHD flow through a porous medium with variable temperature in presence of heat source/sink is studied by Vijaya Kumar et al. [11]. Vijaya sekhar and Viswanadh reddy [12] have obtained the analytical solution for the effects of heat sink and chemical reaction on MHD free convective oscillatory flow past a porous plate with viscous dissipation. Gireesh Kumar and Satyanarayana [13] studied the heat and mass transfer effects on unsteady MHD free convective walter's memory flow with constant suction in presence of heat sink. Choudhury and Paban Dhar [14] investigated the effects of MHD Visco-elastic fluid past a moving plate with double diffusive convection in presence of heat generation/absorption.

The objective of the present paper is to analyze the radiation and mass transfer effects on an unsteady two-dimensional laminar convective boundary layer flow of a viscous, incompressible, chemically reacting fluid along a semi-infinite vertical plate with suction, by taking into account the effects of viscous dissipation in presence of heat source/sink. The equations of continuity, linear momentum, energy and diffusion, which govern the flow field are solved by using finite element technique. The behavior of the velocity, temperature, concentration has been discussed for variations in the governing parameters.

MATHEMATICAL ANALYSIS

An unsteady two-dimensional laminar boundary layer flow of a viscous, incompressible, radiating fluid along a semi-infinite vertical plate in the presence of thermal and concentration buoyancy effects is considered, by taking the effect of viscous dissipation into account. The x'-axis is taken along the vertical infinite plate in the upward direction and the y'-axis normal to the plate.The level of concentration of foreign mass is assumed to be low, So that the Soret and Dufour effects are negligible. Now under Boussinesq's approximation, the flow field is governed by the following equations:

$$\frac{\partial v'}{\partial y'} = 0 \tag{1}$$

$$\frac{\partial u'}{\partial t'} + v'\frac{\partial u'}{\partial y'} = \nu \frac{\partial^2 u'}{\partial y'^2} + g\beta(T - T_\infty) + g\beta^*(C - C_\infty) \tag{2}$$

$$\frac{\partial T}{\partial t'} + v'\frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y'^2} - \frac{1}{\rho\, c_p}\frac{\partial q_r}{\partial y'} + \frac{\mu}{\rho\, c_p}\left(\frac{\partial u'}{\partial y'}\right)^2 + \frac{S'(T - T_\infty)}{\rho\, c_p} \tag{3}$$

$$\frac{\partial C}{\partial t'} + v'\frac{\partial C}{\partial y'} = D\frac{\partial^2 C}{\partial y'^2} - k_r'^2 (C - C_\infty) \tag{4}$$

Where u', v' are the velocity components in x', y' directions respectively. t' - the time, ρ -the fluid density, ν - the kinematic viscosity, c_p - the specific heat at constant pressure, g -the acceleration due to gravity, β and β^* - the thermal and concentration expansion coefficient respectively, T - the dimensional temperature, C - the dimensional concentration, α -the fluid thermal diffusivity, μ - coefficient of viscosity, D - the mass diffusivity, k_r' - the chemical reaction parameter.

The boundary conditions for the velocity, temperature and concentration fields are

$$u' = U_0, \quad T = T_w + \varepsilon(T_w - T_\infty)e^{n't'}, \quad C = C_w + \varepsilon(C_w - C_\infty)e^{n't'} \quad \text{at} \quad y' = 0$$
$$u' \to 0, \quad T \to T_\infty, \; C \to C_\infty \quad \text{as} \quad y' \to \infty \tag{5}$$

Where U_0 is the scale of free stream velocity, T_w and C_w are the wall dimensional temperature and concentration respectively, T_∞ and C_∞ are the free stream dimensional temperature and concentration respectively, n' - the constant.
By using Rosseland approximation, the radiative heat flux is given by

$$q_r = -\frac{4\sigma_s}{3K_e}\frac{\partial T^4}{\partial y'} \tag{6}$$

Where σ_s - the Stefan-Boltzmann constant and K_e - the mean absorption coefficient. It should be noted that by using Rosseland approximation, the present analysis is limited to optically thick fluids. If temperature differences within the flow are sufficient, small, then equation(6) can be linearised by expanding T^4 in the Taylor series about T_∞, which after neglecting higher order terms take the form

$$T^4 \approx 4T_\infty^3 T - 3T_\infty^4 \tag{7}$$

In view of equations (6) and (7), equation (3) reduces to

$$\frac{\partial T}{\partial t'} + v'\frac{\partial T}{\partial y'} = \frac{k}{\rho\, c_p}\frac{\partial^2 T}{\partial y'^2} + \frac{16\sigma_s}{3\rho\, c_p K_e}T_\infty^3\frac{\partial^2 T}{\partial y'^2} + \frac{\mu}{\rho\, c_p}\left(\frac{\partial u'}{\partial y'}\right)^2 + \frac{S'(T - T_\infty)}{\rho\, c_p} \tag{8}$$

From the continuity equation (1), it is clear that suction velocity normal to the plate is either a constant or function of time. Hence, it is assumed in the form

$$v' = -V_0\left(1 + \varepsilon\, Ae^{n't'}\right) \tag{9}$$

Where A is a real positive constant, ε and εA are small values less than unity and V_0 is scale of suction velocity at the plate surface.

In order to write the governing equations and the boundary condition in dimension less form, the following non- dimensional quantities are introduced.

$$u = \frac{u'}{U_0},\quad y = \frac{V_0 y'}{\nu},\quad t = \frac{V_0^2 t'}{\nu},\quad n = \frac{\nu n'}{V_0^2},\quad \theta = \frac{T - T_\infty}{T_w - T_\infty},\quad \phi = \frac{C - C_\infty}{C_w - C_\infty}$$
$$\Pr = \frac{\nu\,\rho\, C_p}{k} = \frac{\nu}{\alpha},\quad Sc = \frac{\nu}{D},\quad Gr = \frac{g\beta\nu(T_w - T_\infty)}{U_0 V_0^2},\quad Gm = \frac{g\beta^*\nu(C_w - C_\infty)}{U_0 V_0^2},$$
$$Ec = \frac{U_0^2}{c_p(T_w - T_\infty)},\quad k_r^2 = \frac{k_r'^2\nu}{V_0^2},\quad R = \frac{16\sigma_s T_\infty^3}{3K_e k},\quad S = \frac{S'\nu}{\rho C_p V_0'^2} \tag{10}$$

In view of the equations (6) - (10), Equations (2) - (4) reduce to the following dimensionless form.

$$\frac{\partial u}{\partial t} - \left(1 + \varepsilon\, Ae^{nt}\right)\frac{\partial u}{\partial y} = \frac{\partial^2 u}{\partial y^2} + Gr\theta + Gm\phi \tag{11}$$

$$\frac{\partial \theta}{\partial t} - \left(1 + \varepsilon\, Ae^{nt}\right)\frac{\partial \theta}{\partial y} = \left(\frac{1+R}{\Pr}\right)\frac{\partial^2 \theta}{\partial y^2} + Ec\left(\frac{\partial u}{\partial y}\right)^2 + S\theta \tag{12}$$

$$\frac{\partial\phi}{\partial t}-\left(1+\varepsilon\, Ae^{nt}\right)\frac{\partial\phi}{\partial y}=\frac{1}{Sc}\frac{\partial^2\phi}{\partial y^2}-k_r^2\phi \tag{13}$$

Where Gr, Gm, Pr, R, Ec, Sc and k_r are the thermal Grashof number , solutal Grashof number, Prandtl number, radiation parameter, Eckert number, Schmidt number and chemical reaction parameter respectively.

The corresponding boundary conditions are

$$u=0.5,\quad \theta=1+\varepsilon\, e^{nt},\quad \phi=1+\varepsilon\, e^{nt}\quad \text{at}\quad y=0$$
$$u\to 0,\quad \theta\to 0,\quad \phi\to 0\qquad \text{as}\quad y\to\infty \tag{14}$$

SOLUTION OF THE PROBLEM

The Galerkin equation for the differential equation (11) becomes

$$\int_{y_j}^{y_k} N^{(e)^T}\left[\frac{\partial^2 u^{(e)}}{\partial y^2}+P\frac{\partial u^{(e)}}{\partial y}-\frac{\partial u^{(e)}}{\partial t}+R\right]dy=0 \tag{15}$$

Where $P=1+\varepsilon A\, e^{nt}$, $R=Gr\theta+Gm\,\phi$

Let the linear piecewise approximation solution

$$u^{(e)}=N_j(y)u_j(t)+N_k(y)u_k(t)=N_ju_j+N_ku_k$$

Where $N_j=\dfrac{y_k-y}{y_k-y_j}$, $N_k=\dfrac{y-y_j}{y_k-y_j}$

$$\left.N^{(e)^T}\frac{\partial u^{(e)}}{\partial y}\right\}_{y_j}^{y_k}-\int_{y_j}^{y_k}\left\{\frac{\partial N^{(e)^T}}{\partial y}\frac{\partial u^{(e)}}{\partial y}-N^{(e)^T}\left(P\frac{\partial u^{(e)}}{\partial y}+\frac{\partial u^{(e)}}{\partial t}-R\right)\right\}dy=0 \tag{16}$$

Neglecting the first term in Equation (16) we gets

$$\int_{y_j}^{y_k}\left\{\frac{\partial N^{(e)^T}}{\partial y}\frac{\partial u^{(e)}}{\partial y}-N^{(e)^T}\left(P\frac{\partial u^{(e)}}{\partial y}-\frac{\partial u^{(e)}}{\partial t}+R\right)\right\}dy=0$$

$$\frac{1}{l^{(e)}}\begin{bmatrix}1&-1\\-1&1\end{bmatrix}\begin{bmatrix}u_j\\u_k\end{bmatrix}-\frac{P}{2}\begin{bmatrix}-1&1\\-1&1\end{bmatrix}\begin{bmatrix}u_j\\u_k\end{bmatrix}+\frac{l^{(e)}}{6}\begin{bmatrix}2&1\\1&2\end{bmatrix}\begin{bmatrix}u_j^{\bullet}\\u_k^{\bullet}\end{bmatrix}=R\frac{l^{(e)}}{2}\begin{bmatrix}1\\1\end{bmatrix}$$

Where $l^{(e)}=y_k-y_j=h$ and dot denotes the differentiation with respect to t.

We write the element equations for the elements $y_{i-1}\le y\le y_i$ and $y_i\le y\le y_{i+1_i}$ assemble three element equations, we obtain

$$\frac{1}{l^{(e)}}\begin{bmatrix}1&-1&0\\-1&2&-1\\0&-1&1\end{bmatrix}\begin{bmatrix}u_{i-1}\\u_i\\u_{i+1}\end{bmatrix}-\frac{P}{2}\begin{bmatrix}-1&1&0\\-1&0&1\\0&-1&1\end{bmatrix}\begin{bmatrix}u_{i-1}\\u_i\\u_{i+1}\end{bmatrix}+\frac{l^{(e)}}{6}\begin{bmatrix}2&1&0\\1&4&1\\0&1&2\end{bmatrix}\begin{bmatrix}u_{i-1}^{\bullet}\\u_i^{\bullet}\\u_{i+1}^{\bullet}\end{bmatrix}=R\frac{l^{(e)}}{2}\begin{bmatrix}1\\2\\1\end{bmatrix}$$

Now put row corresponding to the node i to zero, from Equation (16) the difference schemes is

$$\frac{1}{l^{(e)^2}}\left[-u_{i-1}+2u_i-u_{i+1}\right]-\frac{P}{2l^{(e)}}\left[-u_{i-1}+u_{i+1}\right]+\frac{1}{6}\left[\dot{u}_{i-1}+4\dot{u}_i+\dot{u}_{i+1}\right]=R$$

Applying Crank-Nicholson method to the above equation (10), then we gets

$$A_1u_{i-1}^{j+1}+A_2u_i^{j+1}+A_3u_{i+1}^{j+1}=A_4u_{i-1}^{j}+A_5u_i^{j}+A_6u_{i+1}^{j}+P^* \tag{17}$$

Where $A_1=2-6r+3Phr$, $A_2=8+12r$, $A_3=2-6r-3Phr$

$A_4=2+6r-3Phr$, $A_5=8-12r$, $A_6=2+6r+3Phr$

$P^*=12(Gr)k\theta_i^j+12(Gm)k\phi_i^j$;

Applying similar procedure to equation (11) and (12) then we gets

$$B_1\theta_{i-1}^{j+1}+B_2\theta_i^{j+1}+B_3\theta_{i+1}^{j+1}=B_4\theta_{i-1}^{j}+B_5\theta_i^{j}+B_6\theta_{i+1}^{j}+12P^{**}k \tag{18}$$

$$C_1\phi_{i-1}^{j+1}+C_2\phi_i^{j+1}+C_3\phi_{i+1}^{j+1}=C_4\phi_{i-1}^{j}+C_5\phi_i^{j}+C_6\phi_{i+1}^{j} \tag{19}$$

$B_1=3Phr-6Ar-Sk+2$ $B_2=12Ar-4Sk+8$ $B_3=-6Ar-3Phr-Sk+2$

$B_4=6Ar-3Phr+Sk+2$ $B_5=-12Ar+4Sk+8$ $B_6=6Ar+3Phr+Sk+2$

Where $P^{**}=Ec\left(\frac{\partial u}{\partial y}\right)^2$, $A=\frac{1+R}{\Pr}$

Where $C_1=2Sc-6r+3PSc_1rh+Qk$, $C_2=8Sc+12r+4Qk$,

$C_1=2Sc-6r-3PSc_1rh+Qk$

$C_4=2Sc+6r-3PSc_1rh-Qk$ $C_5=8Sc-12r-4Qk$, $C_6=2Sc+6r+3PSc_1rh-Qk$

Here $Q=ScK_r^2$, $r=\frac{k}{h^2}$ and h,k are the mesh sizes along $y-$direction and time $t-$direction respectively. Index i refers to the space and j refers to the time. In Equations (17)-(19), taking i =1(1)n and using initial and boundary conditions(13), the following system of equations are obtained:

$$A_iX_i=B_i \qquad \text{i=1(1)3} \tag{20}$$

Where A_i 's are matrices of order n and X_i,B_i 's column matrices having $n-$components. The solutions of above system of equations are obtained by using Thomas algorithm for velocity, temperature and concentration. Also, numerical solutions for these equations are obtained by C-program. In order to prove the convergence and stability of Galerkin finite element method, the same C-program was run with slightly changed values of h and k and no significant change was observed in the values of u,θ and ϕ . Hence, the Galerkin finite element method is stable and convergent.

The skin-friction, Nusselt number and Sherwood number are important physical parameters for this type of boundary layer flow.

The skin-friction at the plate, which in the non-dimensional form is given by

$$C_f = \frac{\tau'_w}{\rho\, U_0 V_0} = \left(\frac{\partial u}{\partial y}\right)_{y=0} \tag{21)}$$

The rate of heat transfer coefficient, which in the non-dimensional form in terms of the Nusselt number is given by

$$Nu = -x \frac{\left(\dfrac{\partial T}{\partial y'}\right)_{y'=0}}{T_w - T_\infty} \Rightarrow Nu\,\mathrm{Re}_x^{-1} = -\left(\frac{\partial \theta}{\partial y}\right)_{y=0} \tag{22}$$

The rate of heat transfer coefficient, which in the non-dimensional form in terms of the Sherwood number, is given by

$$Sh = -x \frac{\left(\dfrac{\partial C}{\partial y'}\right)_{y'=0}}{C_w - C_\infty} \Rightarrow Sh\,\mathrm{Re}_x^{-1} = -\left(\frac{\partial \phi}{\partial y}\right)_{y=0} \tag{23}$$

Where $\mathrm{Re}_x = \dfrac{V_0 x}{\nu}$ is the local Reynolds number.

RESULTS AND DISCUSSION

In the preceding sections, the problem of an unsteady free convective flow of a viscous, incompressible, radiating and dissipating fluid past a semi- infinite plate with chemically reacting was formulated and solved by finite element technique. The expressions for the velocity, temperature and concentration were obtained. To illustrate the behavior of these physical quantities, numeric values were computed with respect to the variations in the governing parameters viz., the thermal Grashof number Gr, solutal Grashof number Gm , Eckert number Ec, radiation parameter R, Prandtl number $\Pr$, Schmidt number Sc and chemical reaction parameter k_r.

The velocity profiles for different values of the thermal Grashof number Gr are described in fig.1. It is observed that an increase in Gr, leads to arise in the values of velocity. Hence the positive values of Gr corresponds to cooling of the plate. In addition, it is observed that the velocity increases rapidly near the wall of the plate as Grashof number incrases and then decays to the free stream velocity.

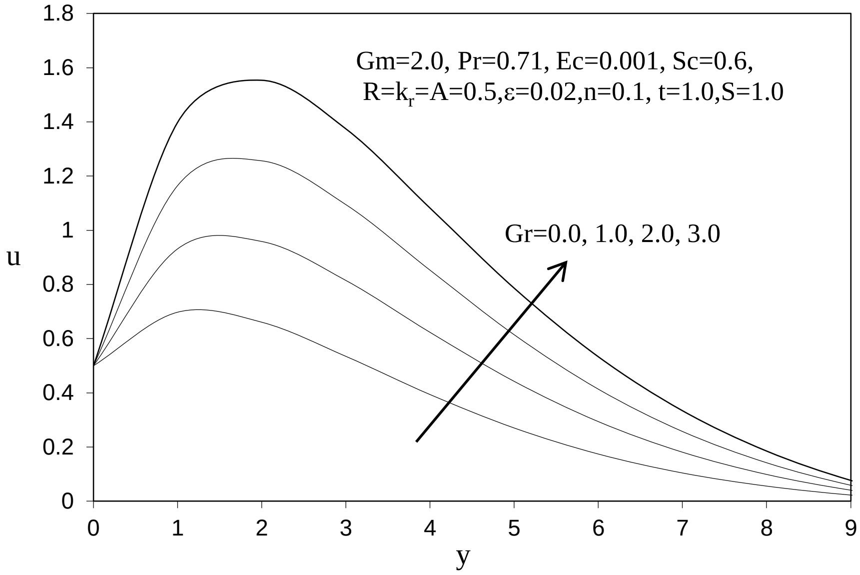

Fig.1. Velocity profiles for different values of Gr

For the case different values of the solutal Grashof number *Gm* , the velocity profiles in the boundary layer are shown in fig.2. It is noticed that an increase in *Gm* , leads to a rise in the values of velocity(S=1.0).

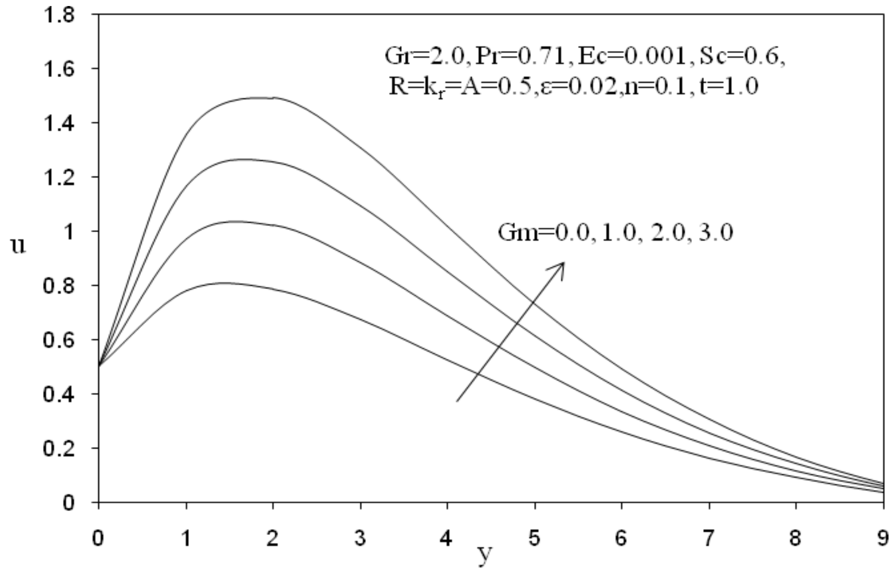

Fig.2. Velocity profiles for different values of Gm

Figs 3(a) and 3(b) shows the velocity and temperature profiles for different values of the Radiation parameter *R* by taking S=1.0 , it is noticed that an increase in the radiation parameter results decrease in the velocity and temperature with in boundary layer, as wellas decreased the thickness of the velocity and temperature boundary layers.

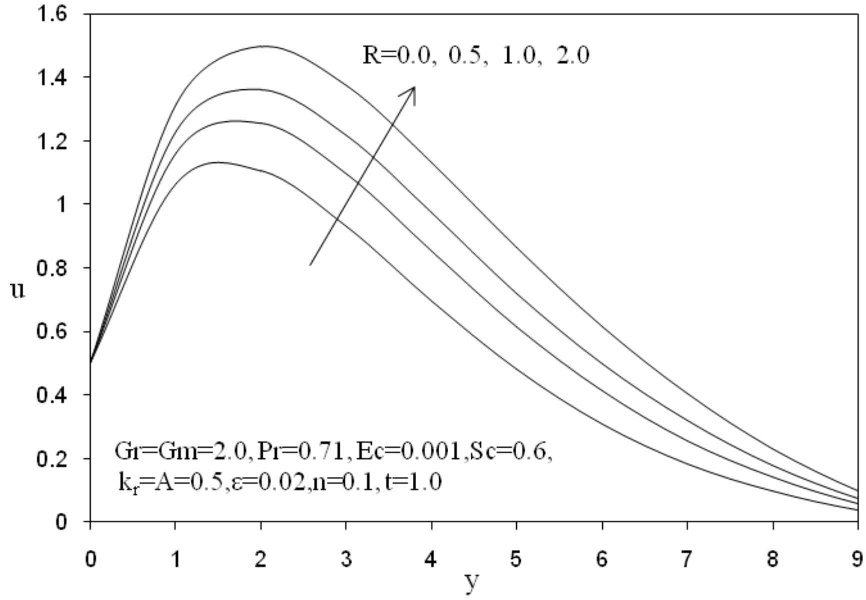

Fig.3(a). velocity profiles for different values of R

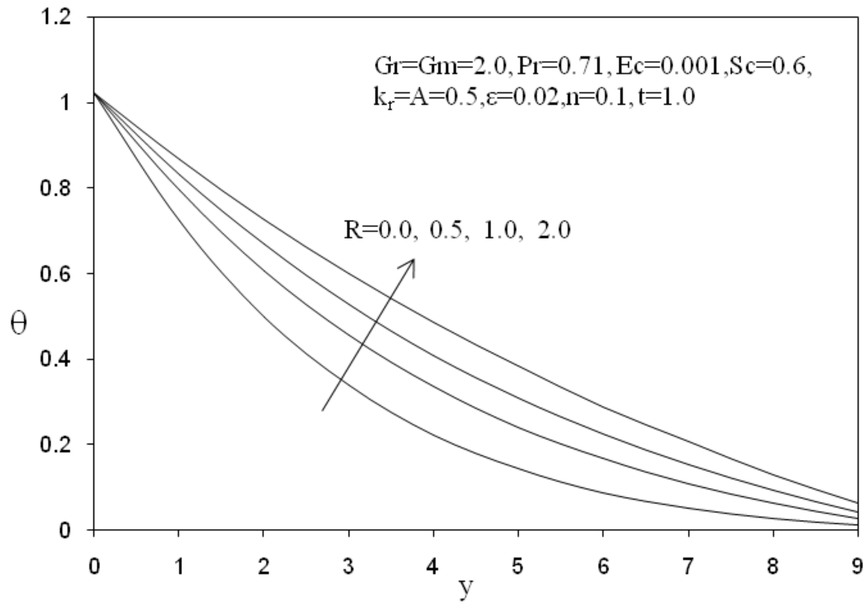

Fig.3(b). Temperature profiles for different values of R

The effects of the viscous dissipation parameter i.e., Eckert number on the the velocity and temperature (S=1.0) are shown in fig.4(a) and fig.4(b). Greater viscous dissipative heat causes a rise in the temperature as well as the velocity.

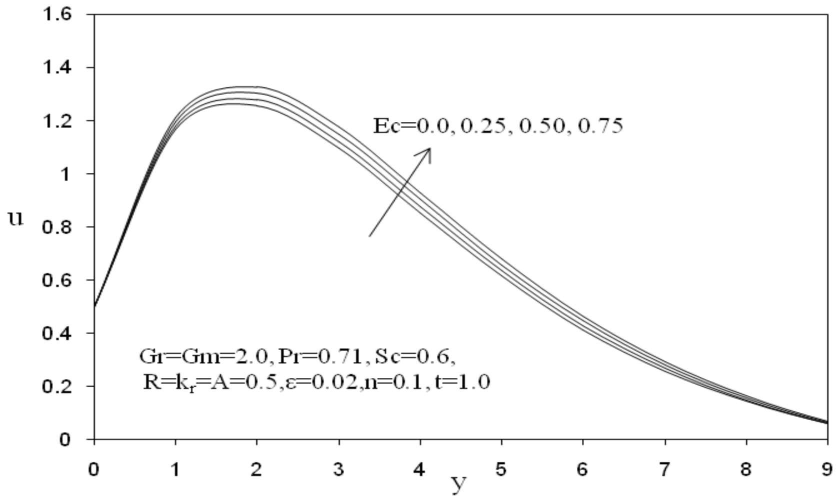

Fig.4(a). Velocity profiles for different values of Ec

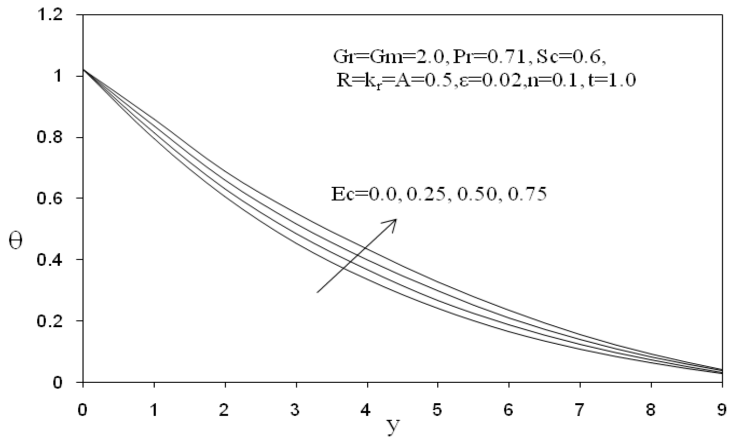

Fig.4(b). Temperature profiles for different values of Ec

The effect of the Prandtl number on the velocity and temperature(S=1.0) are shown in Fig 5(a) and 5(b). As the Prandtl number increases, the velocity and temperature decreases.

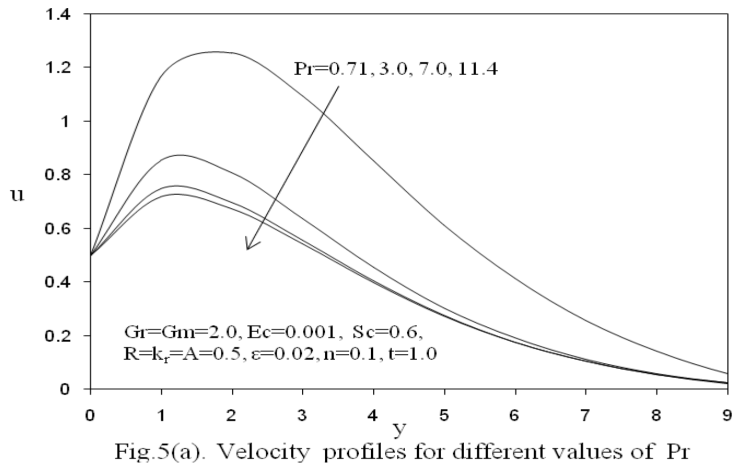

Fig.5(a). Velocity profiles for different values of Pr

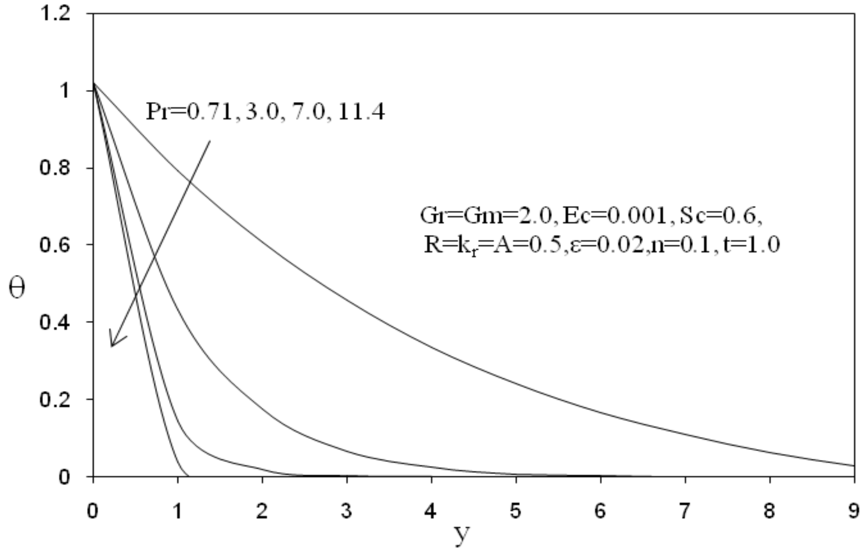

Fig.5(b). Temperature profiles for different values of Pr

The effect of the Schmidt number on the velocity and concentration (S=1.0) are shown in Fig 6(a) and 6(b). As the Schmidt number increases, the velocity and concentration decreases. This causes the concentration buoyancy effects to decrease yielding a reduction in the fluid velocity. Reductions in the velocity and concentration distributions are accompanied by simultaneous reductions in the velocity and concentration boundary layers.

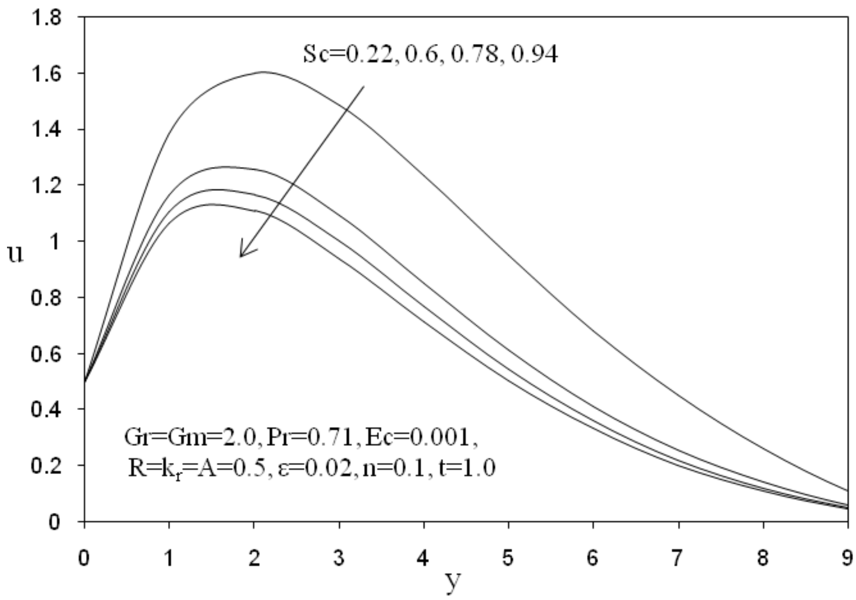

Fig.6(a). Velocity profiles for different values of Sc

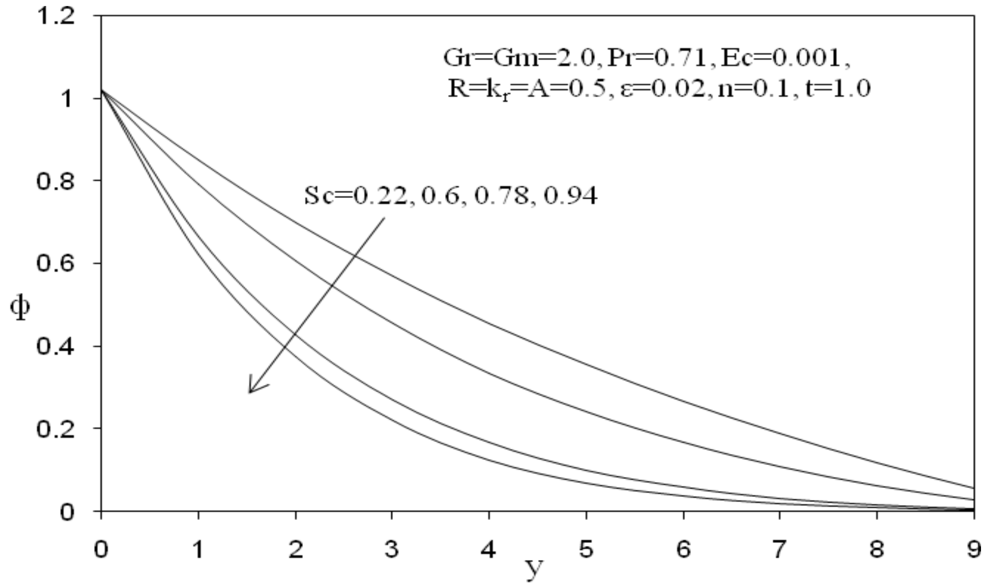

Fig.6(b). Concentration profiles for different values of Sc

Figs. 7(a) and 7(b) illustrates the behavior velocity and concentration for different values of chemical reaction parameter k_r by taking S=1.0 . It is observed that an increase in leads to a decrease in both the values of velocity and concentration.

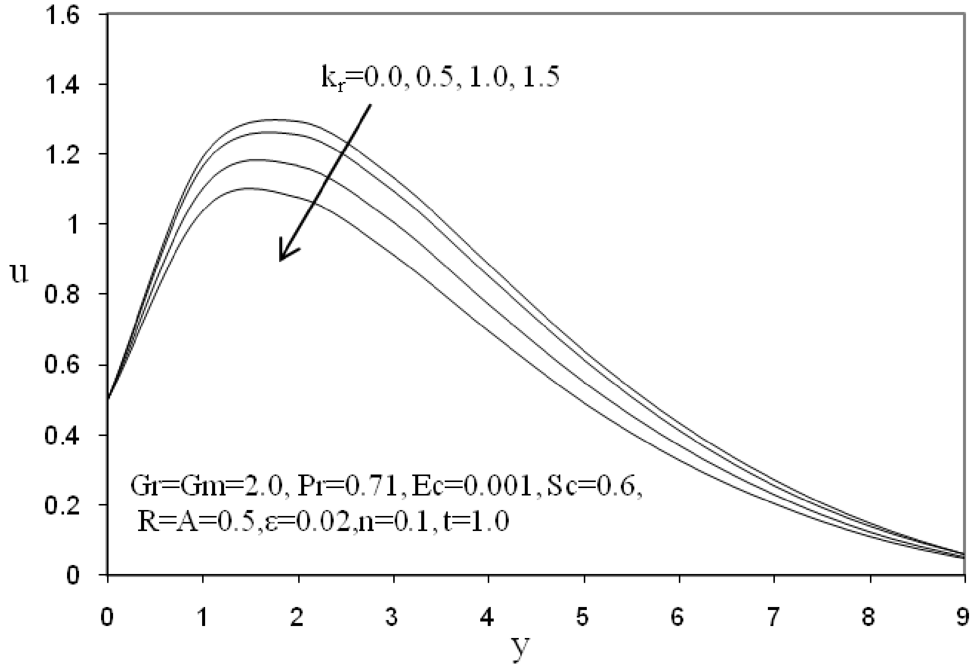

Fig.7(a). Velociyt profiles for different values of k_r

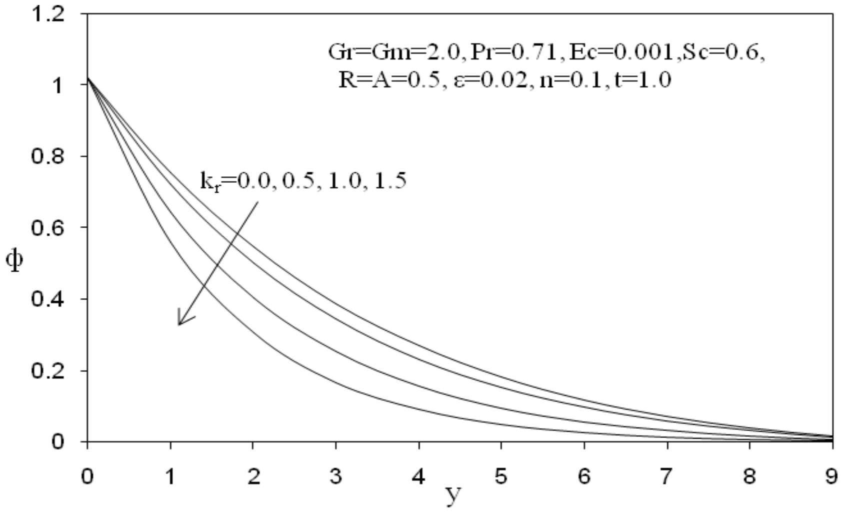

Fig.7(b). Concentration profiles for different values of k_r

Figure 8(a) shows the effects of heat absorption parameter (S) for conducting air(Pr = 0.71) in the case of cooling plate (Gr > 0), i.e., the free convection currents convey heat away from the plate into the boundary layer. With an increase in S from -1.0 (heat absorption) through 0.0 to 1.0 (heat generation), there is a clear increase in the velocity, i.e., the flow is accelerated. When heat is absorbed, the buoyancy force decreases, which retards the flow rate and thereby giving rise to the decrease in the velocity profiles.

The temperature profiles θ are depicted in Fig. 8(b) for different values of heat absorption parameter S the fluid temperature is noticeably enhanced with an increase in S from -1.0 through 0.0 to 1.0. This increase in the temperature profiles is accompanied by the simultaneous increase in the thermal boundary layer thickness.

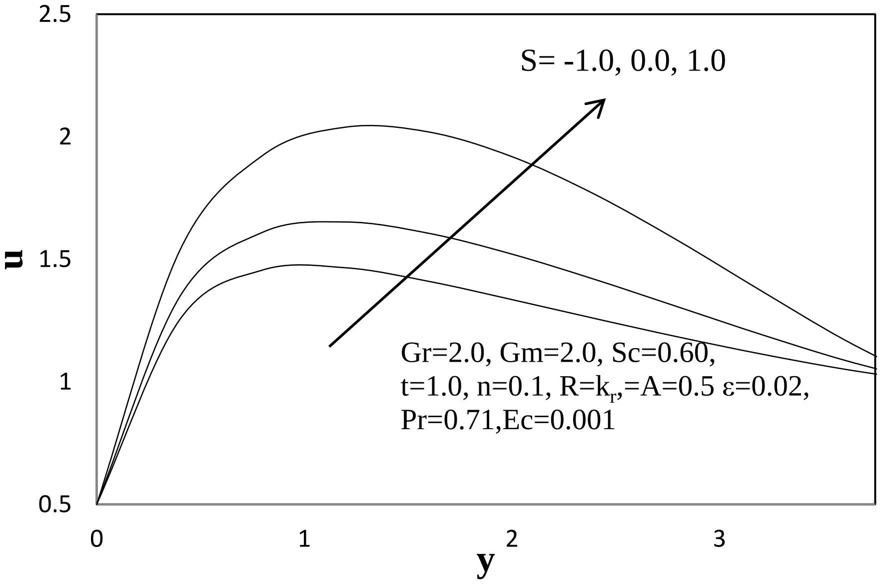

Figure 8(a). Effect of Heat Absorption Parameter ‘S’ onVelocity profiles ‘u’.

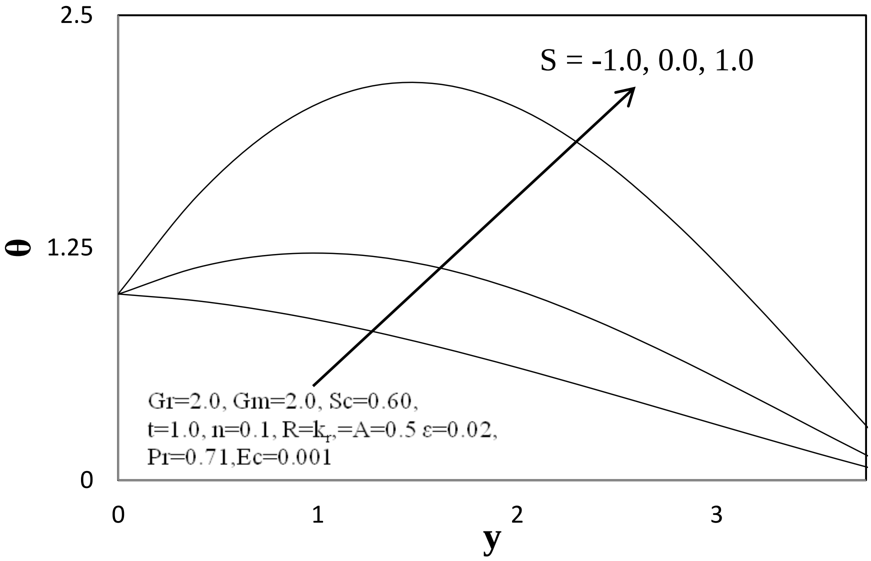

Figure 8(b). Effect of heat absorption parameter ‘S’ on temperature Profiles ‘θ’

Table 1-6 present the effects of the thermal Grashof number, solutal Grashof number, radiation parameter, Schmidt number and Eckert number on the skin-frication coefficient, Nusselt number and Sherwood number. From Tables 1 and 2, it is observed that as Gr or Gm increases, the skin –friction coefficient increases. However, from Table 3, it can be seen that as the radiation parameter increases, the skin-friction coefficient increases and Nusselt number decreases. From Table 4, it is noticed that an increase in the Schmidt number reduces the skin-friction coefficient and increases the Sherwood number. Finally, it is observed from Table 5 that as Eckert number increases, the skin-friction coefficient increases and the Nusselt number decreases. From table 6, it can be seen that as S increases, the skin –friction coefficient increases and Nusselt number decreases.

Table 1: Effect of Gr on C_f

Reference values as in Fig.1.

Gr	C_f
0.0	0.8343
1.0	1.6445
2.0	2.4548
3.0	3.2652

Table 2: Effect of Gm on C_f

Reference values as in Fig.1.

Gm	C_f
0.0	1.0816
1.0	1.7682
2.0	2.4548
3.0	3.1414

Table 3: Effect of R on C_f and Nu

Reference values as in Fig.3(a)

R	C_f	Nu
0.0	2.1664	0.8365
0.5	2.4548	0.6139
1.0	2.6536	0.5032
2.0	2.9037	0.4010

Table 4: Effect of Sc on C_f and Sh

Reference values as in Fig.3(a)

Sc	C_f	Sh
0.22	3.1068	0.4515
0.60	2.4548	0.8431
0.78	2.2767	1.0214
0.94	2.1540	1.1745

Table 5: Effect of Ec on C_f and Nu

Reference values as in Fig.3(a)

Ec	C_f	Nu
0.0	2.4546	0.6143
0.25	2.5010	0.5130
0.50	2.5489	0.4039
0.75	2.5985	0.2863

Table 6: Effect of S on C_f and Nu

Reference values as in Fig.3(a)

S	C_f	Nu
-1.0	2.1224	0.6174
0.0	2.4241	0.5718
1.0	2.6833	0.4649

CONCLUSIONS

We have formulated and solved approximately the problem of two-dimensional fluid flow in the presence of radiative heat transfer, viscous dissipation and chemical reaction parameter. A finite element technique is employed to solve the resulting coupled partial differential equations. The conclusions of the study are as follows:

1. The velocity increases with the increase in thermal Grashof number and solutal Grashof number.
2. An increase in the Eckert number increases the velocity and temperature.

3. An increase in the Prandtl number decreases the velocity and temperature.
4. An increase in the radiation parameter leads to increase in the velocity and temperature.
5. An increase in the heat source/sink parameter leads to increase in the velocity and temperature.
6. The velocity as well as concentration decreases with an increase in the Schmidt number.
7. The velocity as well as concentration decreases with an increase in the chemical reaction parameter.

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